# Incorporating sedimenttransport capabilities to DSM2

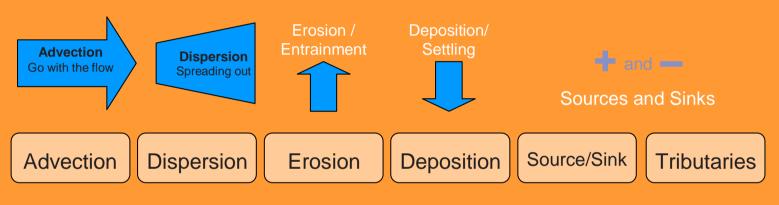
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Technical Advisory Committee, Department of Water Resources, January 13, 2010



## **Background**



Progress to Date: Single Channel



Next step: Complete single channel model



Next step: Extend model to a channel network

# Modes of sediment transport

#### 1-Bed Load

Background

Mainly empirical formulas Lagrangian solution for each particle

#### 2-Suspended Load

Advection-Dispersion-Sink/Source

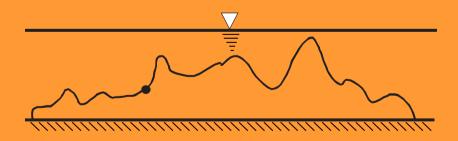
#### 3-Wash Load

There is a third mode of sediment transport called wash load, whereby very fine particles are transported downstream with very little interaction with the bed sediments.

During floods, the wash load is deposited in the floodplains (usually ignored in numerical simulations).







# **Modes of sediment transport**

Sediment transport as bed-load in rivers



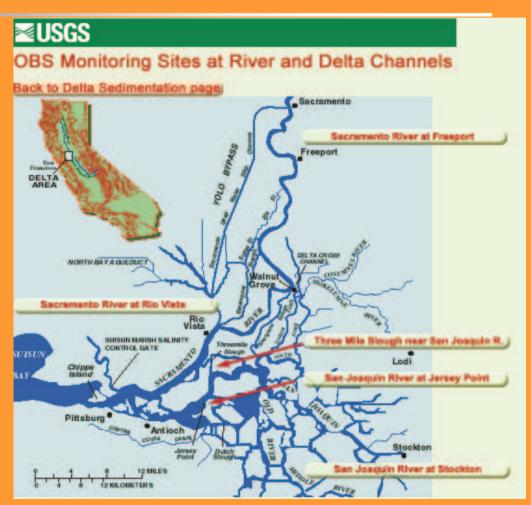
Source: Prof. Dietrich's website

## Modes of sediment transport in the **Delta**

We find the transport of sediment as bed-load and in suspension. Not much information exists about wash load.

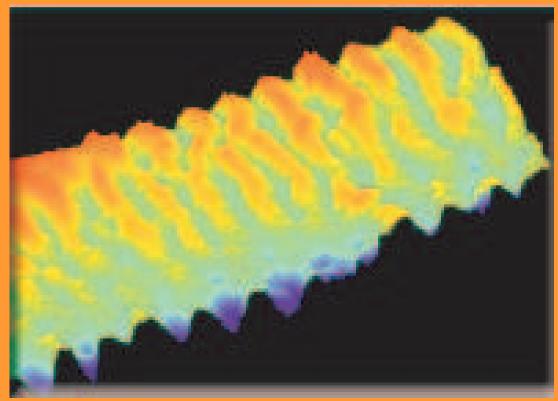
In large portions of the Delta, the sediment can be cohesive.

The USGS has numerous stations in which sediment in suspension is monitored via optical backscatter sensors (OBS).



# **Modes of sediment** transport in the Delta

Bed-forms at Garcia Bend in Winter 2000.

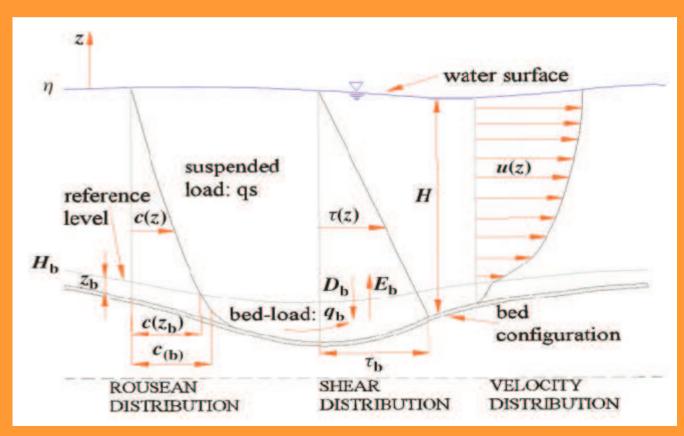


Source: USGS website



# Mathematical treatment of the problem

Tracking individual particles is not feasible for a system of the size of the Delta. Then, we need to use the continuum approach.



Source: Abad et al., 2007



## **Mathematical treatment of problem: Sediment in suspension**

Sediment transport in suspension:

$$\frac{\partial (A C_s)}{\partial t} + \frac{\partial (Q C_s)}{\partial s} = \frac{\partial}{\partial s} \left[ A K_s \frac{\partial C_s}{\partial s} \right] + E - D + q_L C_L + S/S$$

A: cross-sectional wetted area ( $m^2$ )

 $C_s$ : volumetric cross-sectional-averaged concentration of sediment in suspension (-)

Q: flow discharge (m<sup>3</sup>/s)

S/S: non-point sources/sinks (m<sup>2</sup>/s)

 $K_{\circ}$ : dispersion coefficient (m<sup>2</sup>/s)

*E* and *D*: entrainment rate of sediment into suspension and deposition rate of sediment per unit width, respectively (m<sup>2</sup>/s)

 $q_L$  and  $C_L$ : lateral discharge (m<sup>2</sup>/s), and concentration (-), respectively



## Mathematical treatment of the problem: bed-load transport

Sediment transport as bed-load:

$$\frac{q_b}{\sqrt{R \ g \ d_P^3}} = f(excess \ shear \ stress)$$

 $q_h$ : bed-load solid discharge per unit width (m<sup>2</sup>/s)

$$R = \frac{(\rho_s - \rho)}{\rho}$$
: specific gravity (-)

 $d_n$ : sediment particle diameter (m)

g: acceleration of gravity (m/s<sup>2</sup>)

The equation for sediment in suspension comes from the integration in the cross section up to  $z_h$ .



#### **Mathematical treatment of the problem: Entrainment and Deposition**

$$E = E_s \ w_s \ B$$

$$D = C_{sl} w_{s} B$$

 $C_{sl}$ : sediment concentration at the bottom (-)

 $W_{\rm s}$ : settling velocity

Recent developments in sediment transport refer to several active layers, which could be incorporated in a second stage of the model development.



## **Numerical Method: Operator Splitting**

2<sup>nd</sup> order accurate Strang type splitting algorithm

$$c_t = -uc_x + Dc_{xx} + R$$

1) 
$$c_t^* = -uc_x^*$$
  $c^*(t_n, x) = c(t_n, x), \qquad t \in [t_n, t_{n+\frac{1}{2}}]$ 

2) 
$$c_t^{**} = Dc_x^{**} + R$$
  $c_t^{**}(t_n, x) = c_t^{*}(t_{n+\frac{1}{2}}, x), \quad t \in [t_n, t_{n+1}]$ 

3) 
$$c_t^* = -uc_x^*$$
  $c_t^*(t_n, x) = c_t^{**}(t_n, x), \quad t \in [t_{n+\frac{1}{2}}, t_{n+1}]$ 



#### **Numerical Method: Diffusion**

**2nd order, implicit**  $\frac{\partial (AC_s)}{\partial t} = \frac{\partial}{\partial r} (AK_s \frac{\partial C_s}{\partial r})$ 

$$\frac{\partial (AC_s)}{\partial t} = \frac{\partial}{\partial x} (AK_s \frac{\partial C_s}{\partial x})$$

$$\left(\frac{-\theta \Delta t}{\Delta x^{2}}(AK_{s})_{i-\frac{1}{2}}^{n+1} - A_{i}^{n+1} + \frac{\theta \Delta t}{\Delta x^{2}}(AK_{s})_{i+\frac{1}{2}}^{n+1} + \frac{\theta \Delta t}{\Delta x^{2}}(AK_{s})_{i-\frac{1}{2}}^{n+1} - \frac{\theta \Delta t}{\Delta x^{2}}(AK_{s})_{i+\frac{1}{2}}^{n+1}\right)_{1 \ge 3} \times \begin{pmatrix} C_{i-1}^{n+1} \\ C_{i}^{n+1} \\ C_{i+1}^{n+1} \end{pmatrix}_{3 \le 1} = 0$$

$$\left( (AC_s)_i^n + \frac{(1-\theta)\Delta t}{\Delta x^2} \left\{ (AK_s)_{i+\frac{1}{2}}^n (C_s)_{i+1}^n - (AK_s)_{i+\frac{1}{2}}^n (C_s)_i^n - (AK_s)_{i-\frac{1}{2}}^n (C_s)_i^n + (AK_s)_{i-\frac{1}{2}}^n (C_s)_{i+1}^n \right\} \right)_{1 \times 1}$$

Neumann boundary condition:  $\frac{\overline{C_{S/2}^{n+1} - C_{S/0}^{n+1}}}{2\Delta x} = s^{n+1} \qquad O(\Delta x^2)$ 

Dirichlet boundary condition:  $C_s^{n+1}$  is known



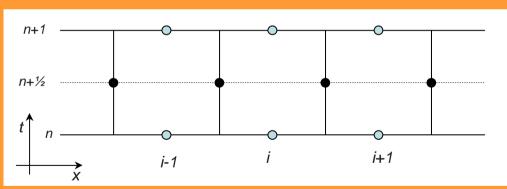
#### **Numerical Method: Advection**

2<sup>nd</sup> order explicit 
$$\frac{\partial (AC_s)}{\partial t} + \frac{\partial (QC_s)}{\partial x} = \frac{\partial}{\partial x} \left( AK_s \frac{\partial (C_s)}{\partial x} \right) + S/S = D + S/S$$

1) 
$$\overline{C}_{i\pm 1/2}^{n+1/2} = C_i^n + \frac{\partial C_i^n}{\partial x} \frac{\Delta x}{2} + \frac{\partial C_i^n}{\partial t} \frac{\Delta t}{2} = C_i^n + \frac{1}{2} \left( \pm 1 - \frac{\Delta t}{\Delta x} \frac{Q}{A} \right) \Delta C_i^n$$

$$\begin{cases} \Delta C_i^n = \frac{\partial C}{\partial x} \Delta x = D \left( C_{\text{lim ited}} \right)_i^n \Delta x & n+1 \\ D \left( C_{\text{lim ited}} \right)_i^n = Limited & flux & n+\frac{1}{2} \end{cases}$$

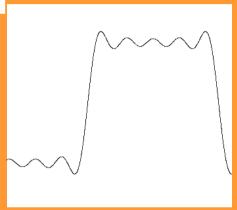
2) 
$$C_{i\pm 1/2}^{n+1/2} = \overline{C}_{i\pm 1/2}^{n+1/2} + \frac{\Delta t}{2A} (S_i^n + D_i^n)$$
  $\xrightarrow{t \cap n}$   $\xrightarrow{i-1}$ 



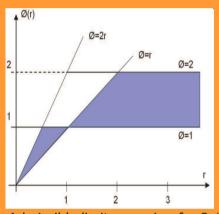
3) 
$$AC_{i}^{n+1} = AC_{i}^{n} - \Delta t \times \frac{QC_{i+\frac{1}{2}}^{n+\frac{1}{2}} - QC_{i-\frac{1}{2}}^{n+\frac{1}{2}}}{\Delta x} + \frac{\Delta t}{2} \times \left[S(C_{i}^{n}) + S(\overline{C}_{i}^{n+1})\right]$$



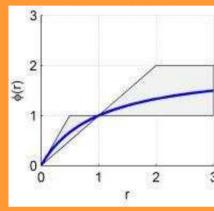
#### **Numerical Method: Flux limiter**



Gibbs phenomenon



Admissible limiters region for 2<sup>nd</sup> order schemes (Sweby 1984)



van Leer limiter (1974)

$$F\left(u_{i+\frac{1}{2}}\right) = f_{i+\frac{1}{2}}^{low} - \phi\left(r_{i}\right) \left(f_{i+\frac{1}{2}}^{low} - f_{i+\frac{1}{2}}^{high}\right)$$

$$F\left(u_{i-\frac{1}{2}}\right) = f_{i-\frac{1}{2}}^{low} - \phi\left(r_{i-1}\right) \left(f_{i-\frac{1}{2}}^{low} - f_{i-\frac{1}{2}}^{high}\right).$$

$$\begin{cases} r_i = \frac{C_i - C_{i-1}}{C_{i+1} - C_i} \\ \phi = \left\lceil \frac{r + |r|}{1 + |r|} \right\rceil & (van \ Leer \ 1974) \end{cases}$$



## **Test: Mesh Convergence**

#### Norms as measure of functions

$$L_{\infty} = ||\vec{v}||_{\infty} = \max_{i} v_{i}|$$

(The most restrictive norm)

$$L_{1} = \frac{\sum_{j} \|\vec{v}\|_{1}}{n} = \frac{\sum_{j}^{n} \sum_{i} |v_{i}|}{n}$$

$$L_2 = \frac{\sum_{j}^{n} \left(\sum_{i} |v_i|^2\right)^{\frac{1}{2}}}{n}$$

(The less restrictive norm )



Background

# **Test: Mesh Convergence II**

								1			
`Table 1: Errors and Norm of Errors in Different Mesh Sizes for ⊖=0.5											
Num of volumes	П	Rate of L1 change	L2	Rate of L2 change	۳٦	Rate of L∞ change	Ddt/dx²	Stability			
25	2.030E-03	1.094E+00	8.407E-07	5.355E+00	3.622E-04	3.844E+00	3.858E-01	O.K			
50	1.855E-03	1.025E+00	1.570E-07	5.797E+00	9.422E-05	4.090E+00	1.482E+00	O.K			
100	1.809E-03	1.006E+00	2.708E-08	5.760E+00	2.304E-05	4.072E+00	6 050E+00	O.K			
200	1.798E-03	1.001E+00	4.701E-09	5.845E+00	5.657E-0	4.151E+00	2 445E+01	O.K			
400	1.796E-03	1.000E+00	8.044E-10	6.301E+00	1.363E-06	4.611E+00	.827E+01	O.K			
800	1.795E-03	1.993E+00	1.277E-10	6.708E+00	2.956E-07	3.385E+00	3.941E+02	O.K			
1600	9.008E-04	1.002E+00	1.903E-11	1.518E+00	8.732E-08	1.0005+00	1.578E+03	O.K			
3200	8.991E-04	х	1.254E-11	х	8.732E-08	Х	6.317E+03	O.K			

# **Tests: Analytical Solutions I** (Diffusion)

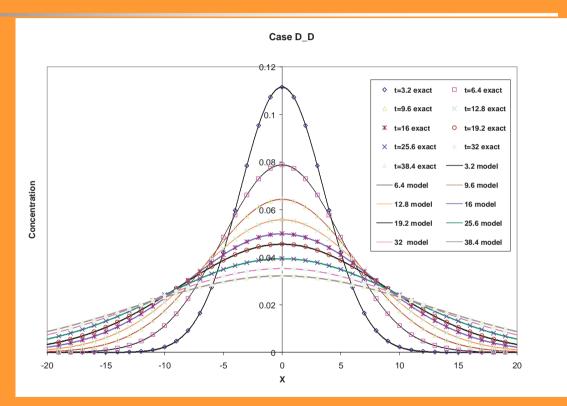
$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

Subject to:

I.C. 
$$C(x,0) = \delta(x) = \begin{cases} \infty, & x = 0 \\ 0, & x \neq 0 \end{cases}$$

$$B.C.$$
  $x \rightarrow \pm \infty$ :  $C(x,t) = 0$ 

$$C_{exact}(x,t) = \frac{e^{-\frac{x^2}{4Dt}}}{\sqrt{4\pi Dt}}$$

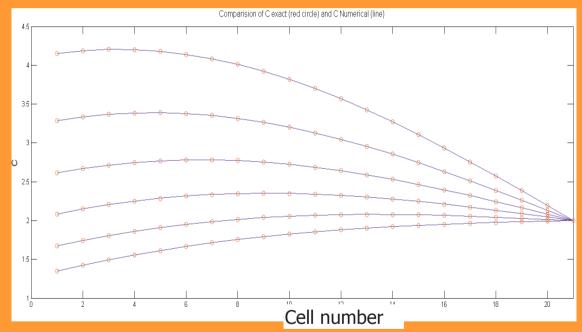


# **Tests: Analytical Solutions II** (Diffusion)

$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

Subjected to:

I.C.: 
$$c(x,0) = 2x + 4\cos\left(\frac{\pi x}{2}\right)$$



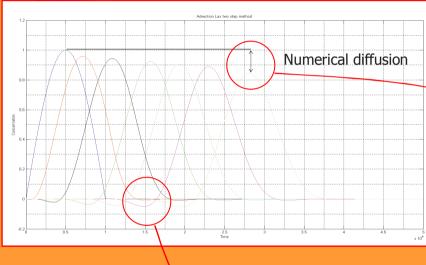
B.C. 
$$(x = 0.1)$$
:  $\frac{\partial c}{\partial x} = 2 - 2\pi \sin(0.05\pi) \exp\left[-D\left(\frac{\pi}{2}\right)^2 t\right]$  Neumann

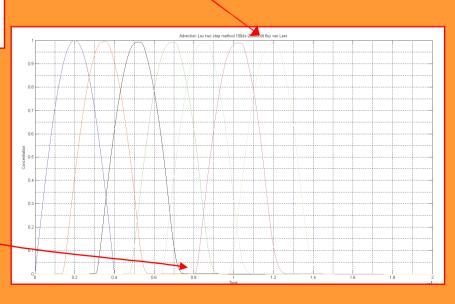
(x = 1): c(1,t) = 2 Dirichlet

$$c_{exact}(x,t) = 2x + 4\cos(0.5\pi x)\exp\left[-D\left(\frac{\pi}{2}\right)^2 t\right]$$



### **Tests: Advection**



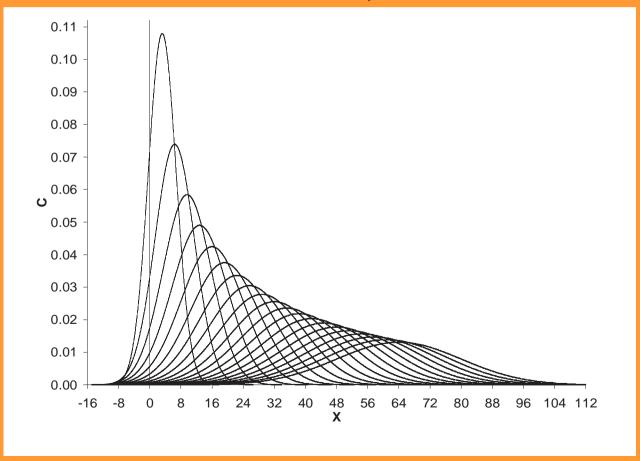




# Tests: A-D-R (to be included)

Source: McDonald, 2007

$$c = \frac{e^{-\lambda t - \frac{(x - ut)^2}{4Dt}}}{\sqrt{4\pi Dt}}$$



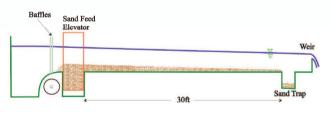


# **Tests: Experimental Data I** (to be done)

Comparison with experimental lab data

Newton (1951).

Exp.	Flow Discharge	Sediment Size	Initial Bed	Initial	Final	Duration
	$(m^3/s)$	(mm)	Slope (m/m)	$n_b$	n <sub>b</sub>	(hour)
Run 1	0.00566	0.69	0.0046	0.016	0.012	24
Run 3	0.00566	0.69	0.0061	0.016	0.012	27



Configuration of Newton's (1951) Experiment

Measured by Newton (1951) Calculated, with Wu et al. Formula Calculated, with Ackers-White Formula Sediment Discharge at Outlet (kg/s) 0.002 Time (hr)

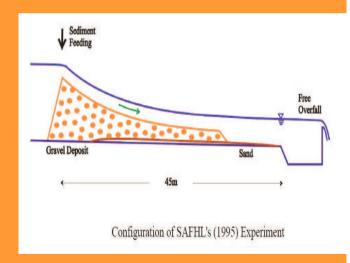
Sediment Discharges at Outlet for Newton's Exp. Run 1

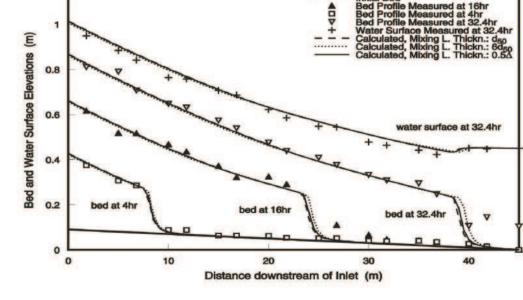


# **Tests: Experimental Data II** (to be done)

Comparison with experimental lab data

Cui et al. (1995/6).





Sensitivity of Bed Profile to Mixing Layer Thickness (SAFHL's Experiment Run 2)



# **Question: Physical Bed roughness**

- $K_s = K_s''(skin friction) + K_s''(form drag)$
- 1-Methods based on bed-forms and grain-related parameters such as bed-form length, height, steepness and bed-material size:

$$K'_{s}$$
 min= 0.01 m  
 $K'_{s}$  = 3 d<sub>90</sub> for  $\theta$  <1 (lower regime)  
 $K'_{s}$  = 3  $\theta$  d<sub>90</sub> for  $\theta$  >1 (upper regime)

- Is there information on  $d_{90}$ ,  $d_{50}$ , and  $\Delta$  available for the Delta?
- 2-Methods based on integral parameters such as mean depth, mean velocity and bed material size

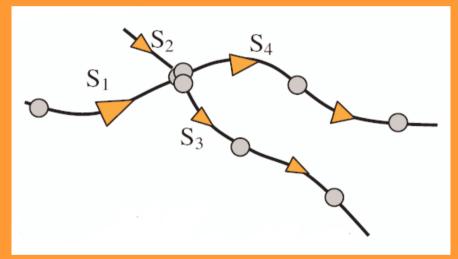
$$k_{s,c} = d_{50}[1 + 700(\theta - \theta_{cr})]$$

$$\theta = \frac{\tau_b}{((\rho_s - \rho)gd_{50})}$$
 mobility parameter



#### **Question: Physical – Distribution in Junctions**

• Do you know of any studies of sediment transport at junctions in the Delta or in other systems?



Source: Mike11, DHI

$$S_3 = \frac{K_3 Q_3^{n3}}{K_3 Q_3^{n3} + K_4 Q_4^{n4}} (S_1 + S_2)$$



#### **Question: Physical Treatment of Bed-load**

- 1- Solve an advection-diffusion-reaction equation for suspended load, and use empirical formula for computing bed-load
- 2- Solve an advection-diffusion-reaction equation for both the bedload and the suspended load, following the proposal by Greimann et al. (2008):

$$\frac{\partial hC}{\partial t} + \frac{\partial \cos(\alpha)\beta V_t hC}{\partial x} + \frac{\partial \sin(\alpha)\beta V_t hC}{\partial y} = \frac{\partial}{\partial x}(hfD_x \frac{\partial C}{\partial x}) + \frac{\partial}{\partial y}(hfD_y \frac{\partial C}{\partial y}) + S_e$$

S<sub>a</sub>= Erosion source term

f = Transport load parameter, fraction of suspended load to total load

h = Flow depth

a = Angle of sediment transport

b = Ratio of sediment velocity to flow velocity

V<sub>+</sub> = Total flow velocity

# **Question: Physical - Entrainment & Deposition**

- 1-In the Delta, is there any tested method for representation of settling velocity (or deposition instead) for cohesive sediment particles beyond Krone's (1962) work?
- 2-In the Delta, is there any tested expression for entrainment of cohesive sediment  $E = \alpha \left[ \frac{\tau_b - \tau_{cr}}{\tau} \right]^{\beta}$ particles beyond the work by Krone (1962)?
- 3-To reduce the number of variables for description of cohesive sediment, which are the most important variables for the Delta?  $W_s = W_s$  (Salinity, Concentration, ...)
- 4-In the Delta, is there any tested method for representation of settling velocity (or deposition instead) for cohesive sediment particles?
- i)  $W_s = \text{constant}$ , ii)  $W_{s,m} = W_s (1 \text{ac})^b$ , iii)  $W_{s,m} = Kc^m$



# **Question: Numerical**

- 1-Do you know of any reliable second order methods for updating boundary conditions for advectiondiffusion-reaction equations with operator splitting?
- 2-What order, in the splitting procedure, should we solve the advection-diffusion-reaction equations? Our initial thought is to solve advection first, then reaction and finally diffusion. Advection is always the dominant term and it should come first.



# **Questions:** User need/request

- What kinds of analytical tests and comparisons to data (field and laboratory) would you like to see in the STM code?
- What units for sediment/constituent concentration you would like to see in DSM2-STM? Volume per volume or mass per volume?
- Is it desirable for STM to have a feature that allows the user to select the numerical scheme to be used to solve the advection part?
- Initial non-cohesive implementation has:
- 1) Garcia and Parker (1991); 2) van Rijn (1984); 3) Smith and McLean (1977); 4) Zyserman and Fredsoe (1994)

Is there any other formulation you prefer to have in DSM2-STM?

# Thank you!

